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INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

(Chapter II of the Patent Cooperation Treaty)

(PCT Article 36 and Rule 70)

Applicant's or agent's file reference SKF120011505	FOR FURTHER ACTION	See Form PC	T/IPEA/416
	International filing date (day/mo	onth/year) I	Priority date (day/month/year)
International application No.	04.07.2002		10.07.2001
PCT/FI 2002/000611 International Patent Classification (IPC) or			
D21C 11/12	induonal viaconal		1
0210 11/12			
Applicant			
Fortum OYJ et al			
This report is the international pre Authority under Article 35 and to	climinary examination report, esta	ablished by this ling to Article 36	International Preliminary Examining 5.
2. This REPORT consists of a total		ding this cover s	heet.
3. This report is also accompanied b			
	and to the International Bureau)) a total of 2	sheets, as follows:
sheets of the and/or sheets	description, claims and/or drawing containing rectifications authorized	and which have	been amended and are the basis of this report cority (see Rule 70.16 and Section 607 of the
	isclosure in the international appl	ich this Authorit lication as filed,	y considers contain an amendment that goes as indicated in item 4 of Box No. I and the
	onal Bureau only) a total of (indi	icate type and ni	umber of electronic carrier(s))
-	containing a ce	emence listing a	nd/or tables related thereto, in computer
readable form only, Administrative Instr	as indicated in the Supplemental	Box Relating to	Sequence Listing (see Section 802 of the
4. This report contains indications	relating to the following items:		
Box No. I Basis	of the report		
Box No. II Priorit			and a second continuities
Box No. III Non-e	stablishment of opinion with rega	ard to novelty, i	nventive step and industrial applicability
	of unity of invention		
applic	ability; citations and explanation	2) with regard to as supporting suc	novelty, inventive step or industrial th statement
	in documents cited		
	in defects in the international app		
Box No. VIII Certa	in observations on the internation		
Date of submission of the demand	Dat	te of completion	of this report
09.01.2004).10.2004	
Name and mailing address of the IPEA	/SE	thorized officer	
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International application No.

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Box	No. I	Basis of the report	
1.	otherwi	gard to the language, this report is based on the international applicated under this item.	
1		This report is based on a translation from the original language into the swhich is the language of a translation furnished for the purposes of:	following language,
		international search (under Rules 12.3 and 23.1(b))	
		publication of the international application (under Rule 12.4)	
		international preliminary examination (under Rules 55.2 and/or	r 55.3)
2.	furnish	egard to the elements of the international application, this report is ed to the receiving Office in response to an invitation under Article 14 to annexed to this report):	s based on (replacement sheets which have been 4 are referred to in this report as "originally filed"
		the international application as originally filed/furnished	
}	\boxtimes	the description:	as originally filed/furnished
]		pages 1 - 11 pages* received by this A	Authority on
		pages* received by this A	Authority on
	5-3	pages*	
	\boxtimes	the claims:	as originally filed/furnished
		pages* as amer	nded (together with any statement) under Article 19
		received by this A	Authority on 11.06.2004
		pages* received by this A	Authority on
	\square	the drawings:	1
		nores 1 - 2	as originally filed/furnished
į		pages* received by this	Authority on
		pages* received by this	Authority on
		a sequence listing and/or any related table(s) – see Supplemental Box	Relating to Sequence Listing.
3.		The amendments have resulted in the cancellation of:	
		the description, pages	
		the claims, Nos.	
		the drawings, sheets/figs	
Ì		the sequence listing (specify):	
1		any table(s) related to the sequence listing (specify):	
4	. 🔲	This report has been established as if (some of) the amendments made, since they have been considered to go beyond the disclosure 70.2(c)).	the this remort and listed below had not been
1		the description, pages	
		the claims, Nos.	
		the drawings, sheets/figs	
		the sequence listing (specify):	
1		any table(s) related to the sequence listing (specify):	
	* If it	em 4 applies, some or all of those sheets may be marked "superseded."	

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Box 1	No. IV Lack of unity of invention
1.	In response to the invitation to restrict or pay additional fees the applicant has:
	restricted the claims.
	paid additional fees.
	paid additional fees under protest.
	neither restricted nor paid additional fees.
2.	This Authority found that the requirement of unity of invention is not complied with and chose, according to Rule 68.1, not to invite the applicant to restrict or pay additional fees.
3.	This Authority considers that the requirement of unity of invention in accordance with Rules 13.1, 13.2 and 13.3 is:
	complied with.
	not complied with for the following reasons:
	The following separate inventions were identified:
	I: Claim 1 is directed to a method for treatment of spent liquor at a pulp mill, which liquor contains sulphur compounds derived from the cooking chemicals. The method is especially suitable for the treatment of black liquor.
	II: Claim 6 is directed to a method for treatment of spent liquor at a pulp mill, which liquor results from cooking with an organic solvent.
	The present application has been considered to contain two inventions which are not linked such that they form a single general inventive concept, as required by Rule 13 PCT for the following reasons:
	The problem to be solved by the invention I is to provide a method for the treatment of spent pulping liquor, containing inorganic cooking chemicals. The method comprises pyrolisation of the spent pulping liquor and a subsequent gasification step, whereupon the cooking chemicals are recovered from the coke thus produced.
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	 Consequently, this report has been established in respect of the following parts of the international application:
	all parts.
	the parts relating to claims Nos.

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Supplemental Box

In case the space in any of the preceding boxes is not sufficient.

Continuation of: Box IV

The problem to be solved by the invention II is to provide a method for the treatment of spent pulping liquor, derived from cooking with an organic solvent. The method comprises pyrolisation of the spent pulping liquor, whereupon the cooking chemicals, i.e. the organic solvent, are recovered from the evaporable compounds produced in the pyrolisation.

The only common technical feature unifying claim 1 and claim 6, is the use of pyrolysis as one sub-step for treatment of spent liquor at a pulp mill.

However, the teaching that pyrolysis can be used for the treatment of spent pulping liquor is previously known from document US 4135968.

Consequently, neither the problems underlying the subjects of the two claimed inventions, nor their solutions, allow for a relationship to be established between the said inventions, which involves a single general inventive concept in the sense of Rule 13.1 PCT

No other features can be distinguished which can be considered as same or corresponding special technical features in the sense of Rule 13.2 PCT.

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Supplemental Box

In case the space in any of the preceding boxes is not sufficient. Continuation of: Box $\,V\,$

part of the spent liquor flow arriving from the evaporation plant is taken to the pyrolysis reactor, whereas a second part of the spent liquor flow is taken to a soda recovery boiler.

There is no evidence on file that shows that this distinguishing feature gives rise to an effect in a non obvious manner. Therefore, the problem to be solved by the method of claim 2 can be seen as being to provide an alternative method to the one disclosed in D1.

However, from D2 it is previously known to divide the spent pulping liquor into two flows, whereupon one part is taken to a pyrolysis reactor, and the second part is taken directly to a soda recovery boiler.

It is considered obvious to a person skilled in the art to use the teaching of D2 in a method as the one disclosed in D1, so as to arrive at the invention according to claim 2.Consequently, the method according to claim 2 is considered obvious to a person skilled in the art.

The subject matters of claims 3-5 are also considered obvious to a person skilled in the art, especially since it is previously known from D2 to use the gas produced from the spent liquor in the pyrolysing unit as fuel.

It is also considered obvious to a person skilled in the art to choose the pyrolysis conditions according to the desired products. Consequently, the subject matters according to claims 9 and 10 are considered obvious to a person skilled in the art.

D3 refers to a process for the recovery of energy and kraft pulping chemicals in a system of multiple reactors. The method comprises pyrolysing kraft black liquor at a temperature of not more than 600 C, whereafter the sulphur compounds contained in the char are reduced to sulphide in a heated reducer. The reduced char is leached with an aqueous leaching liquid to leach inorganic salts comprising carbonates and sulphides. The aqueous liquid thus formed is recovered as green liquor. In the reducing step described in D3, gasification also occurs, whereby the reducing step can be

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	was a state of the second of the second to povel	v inventive step or industrial applicability;
Box No. V	Reasoned statement under Article 35(2) with regard to novel	J, Invenerve coop
DOX 1.01	t t t t t t t t t t t t t t t t t t t	
	citations and explanations supporting such statement	

1. Statement

Novelty (N)	Claims Claims	<u>2 - 10</u> 1	YES NO
Inventive step (IS)	Claims Claims	<u>6</u> 1 - 5, 7 - 10	YES NO
Industrial applicability (IA)	Claims Claims	1 - 10	YES NO

2. Citations and explanations (Rule 70.7)

Reference is made to the following documents:

D1: US 3607619 A D2: US 4135968 A D3: US 5174860 A

D1 refers to a process for the treatment of black liquor from kraft pulp mills comprising coking said black liquor at a temperature in the range of about 450 - 700 °F (232 - 371 °C), in the absence of added free oxygen. During the coking process, organic components of the black liquor are decomposed and dehydrated to a carbonized solid or coke which is discharged at the end of the coking period. The discharged coke may be burned to supply heat for the process and to recover chemicals, such as sodium sulfide and sodium carbonate, contained therein.

It is not explicitly stated in D1 that the coke is taken to a gasification reactor for gasification. However, since sodium sulfide is also recovered from the coke in the process described in D1, the same conditions must prevail in the burning process referred to in D1, as in the gasification process referred to in claim 1. Thus, the burning of the coke described in D1 is considered to be equivalent to the gasification of the coke as stated in claim 1.

Consequently, the method according to claim 1 lacks novelty.

The method according to claim 2 differs from D1 in that only a

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Supplemental Box

In case the space in any of the preceding boxes is not sufficient. Continuation of: Box $\,V\,$

seen as a gasification step under reducing conditions. Air is introduced into the fluid bed pyrolyser and used in the pyrolising step for temperature control and as a fluidizing medium.

The invention as defined in claims 1-6 and 9-10 differs from D3 in that the pyrolisation is preformed in the absence of an external gas component.

However, since it is well known in the art to pyrolise spent pulping liquor without the addition of external gases, the invention as defined in claims 1-6 and 9-10 is considered to lack an inventive step also in view of D3.

It is also considered obvious to a person skilled in the art to arrange the pyrolysis reactor for a batch or for a continuous process. Therefore, also the method according to claims 7 and 8 is considered obvious to a person skilled in the art.

The method according to claim 6 differs from the cited documents in that it refers to the recovery of an organic solvent. In the method according to claim 6, the spent liquor is divided into a solids portion and an evaporated portion, and the cooking chemicals, i.e. the organic solvent, is contained in the latter one. None of the documents D1 - D3 teaches a method suitable for treatment of spent liquors resulting from cooking with an organic solvent.

There is no indication in any of the documents, D1-D3, that would lead a person skilled in the art to the method claimed in claim 6. Consequently, the method according to claim 6 is novel and considered to involve an inventive step.

Accordingly, the method according to claim 1 lacks novelty. The method according to claims 2-5 and 7-10 is novel, but considered to lack an inventive step. The method according to claim 6 is novel and considered to fulfill the requirement of inventive step. The invention is industrially applicable.



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Amended Claims

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- 1. Method for treatment of spent liquor at a pulp mill, especially for treatment of black liquor, in order to recover its contents of chemicals and energy, **characterised** in that a spent liquor flow (10) arriving from the evaporation plant is taken to a pyrolysis reactor (1), wherein it is pyrolysed at a temperature of 300-800°C in the absence of an external gas component in order to separate evaporable compounds (12) from the coke (11) remaining in a solid state, whereupon the evaporable compounds (12) are recovered and the coke (11) is taken to a gasification reactor (3) for gasification, which gasification is implemented under such conditions that the sulphur compounds contained in the coke (11) and deriving from the cooking chemicals are reduced to sodium sulphide.
- 2. Method according to claim 1, **characterised** in that only a part of the spent liquor flow (10) arriving from the evaporation plant is taken to the pyrolysis reactor (1), whereas a second part of the spent liquor flow (10) is taken to a soda recovery boiler (3) where it is burnt in order to recover its contents of chemicals and energy.
- 3. Method according to claim 1 or 2, **characterised** in that the evaporable compounds (12) separated from the spent liquor in the pyrolysis reactor (1) are used at the mill as fuel in part or entirely.
- 4. Method according to claim 1 or 2, **characterised** in that the evaporable compounds (12) separated from the spent liquor in the pyrolysis reactor (1) are processed further.
 - 5. Method according to claim 1 or 2, characterised in that the product gases (14) resulting from the gasification are used at the mill as fuel in part or entirely.
 - 6. Method for treatment of spent liquor at a pulp mill in which cooking is carried

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out with an organic solvent in order to recover its contents of chemicals and energy, **characterised** in that the spent liquor flow (10) arriving from the evaporation plant is taken to a pyrolysis reactor (1), wherein it is pyrolysed at a temperature of 300-800°C in the absence of an external gas component in order to separate evaporable compounds (12) from the coke (11) remaining in a solid state, whereupon the evaporable compounds are recovered and used at the mill as process chemicals in part or entirely, and the coke is taken to a fluidised-bed boiler or some other combustion equipment (4) for burning in order to recover the energy content of the coke.

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7. Method according to any one of claims 1-6, **characterised** in that the pyrolysis reactor (1) is for a batch process, whereby increasing of the temperature may begin from the temperature of the spent liquor arriving in the reactor, while the final temperature is chosen according to the desired final products.

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8. Method according to any one of claims 1-6, characterised in that the pyrolysis reactor (1) is for a continuous process.

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9. Method according to any one of claims 1-8, **characterised** in that the pyrolysis is carried out in such process conditions (temperature, pressure, residence time, heating speed, etc.), wherein the evaporable compounds (12) mainly consist of non-condensing gases.

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10. Method according to any one of claims 1-8, **characterised** in that the pyrolysis is carried out in such process conditions (temperature, pressure, residence time, heating speed, etc.), wherein the evaporable compounds (12) mainly consist of pyrolysis oil.